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## **CLAIMS**

- 1. Solid oxide fuel cell including a cathode, an anode and at least one electrolyte membrane disposed between said anode and said cathode, wherein said anode comprises a cermet including a metallic portion and an electrolyte ceramic material portion, said portions being substantially uniformly interdispersed, said metallic portion having a melting point equal to or lower than 1200°C; said cermet having a metal content higher than 50 wt%, and a specific surface area equal to or lower than 5 m<sup>2</sup>/g.
- 2. Solid oxide fuel cell according to claim 1 wherein the metallic portion is selected from a single metal such as copper, aluminum, gold, praseodymium, ytterbium, cerium, and alloys comprising one or more of these metals together.
- 3. Solid oxide fuel cell according to claim 2 wherein the metallic portion is copper.
- 4. Solid oxide fuel cell according to claim 1 wherein the metallic portion has a melting point higher than 500°C.
- 5. Solid oxide fuel cell according to claim 1 wherein the metal content ranges between 60 wt% and 90 wt%.
  - 6. Solid oxide fuel cell according to claim 1 wherein the cermet has a specific surface area equal to or lower than  $2 \text{ m}^2/\text{g}$ .
  - 7. Solid oxide fuel cell according to claim 1 wherein the cermet has a porosity equal to or higher than 40%
- 8. Solid oxide fuel cell according to claim 1 wherein the ceramic material has a specific conductivity equal to or higher than 0.01 S/cm at 650°C.
  - 9. Solid oxide fuel cell according to claim 8 wherein the ceramic material is selected from, doped ceria and  $La_{1-x}Sr_xGa_{1-y}Mg_yO_{3-\delta}$  wherein x and y are comprised between 0 and 0.7 and  $\delta$  is from stoichiometry.
- 25 10. Solid oxide fuel cell according to claim 9 wherein ceria is doped with gadolinia or samaria.
  - 11. Solid oxide fuel cell according to claim 1 wherein the ceramic material is yttriastabilized zirconia.

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12. Solid oxide fuel cell according to claim 1 wherein the cathode comprises a metal selected from platinum, silver, gold and mixtures thereof, and an oxide of a rare earth element.

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- 13. Solid oxide fuel cell according to claim 1 wherein the cathode comprises a ceramic5 selected from
  - $La_{1-x}Sr_xMnO_{3-\delta}$ , wherein x and y are independently equal to a value comprised between 0 and 1, extremes included and  $\delta$  is from stoichiometry; and
  - $La_{1-x}Sr_xCo_{1-y}FeyO_{3-\delta}$ , wherein x and y are independently equal to a value comprised between 0 and 1, extremes included and  $\delta$  is from stoichiometry.
- 10 14. Solid oxide fuel cell according to claim 13 wherein the cathode comprises doped ceria.
  - 15. Solid oxide fuel cell according to claim 1 wherein the cathode comprises a combination of materials as from claims 12 and 13.
- 16. Solid oxide fuel cell according to claim 1 wherein the electrolyte membrane is selected from yttria-stabilized zirconia, La<sub>1-x</sub>Sr<sub>x</sub>Ga<sub>1-y</sub>MgyO<sub>3-δ</sub> wherein x and y are comprised between 0 and 0.7 and δ is from stoichiometry, and doped ceria.
  - 17. Method for producing energy comprising the steps of:
  - a) feeding at least one fuel into an anode side of a solid oxide fuel cell comprising
- an anode including a cermet comprising a metallic portion and an electrolyte ceramic material portion, said portions being substantially uniformly interdispersed, said metallic portion having a melting point equal to or lower than 1200°C; said cermet having a metal content higher than 50 wt%, and a specific surface area equal to or lower than 5 m<sup>2</sup>/g;
  - a cathode, and
- at least one electrolyte membrane disposed between said anode and said cathode;
  - b) feeding an oxidant into a cathode side of said solid oxide fuel cell; and

- c) oxidizing said at least one fuel in said solid oxide fuel cell, resulting in production of energy.
- 18. Method according to claim 17 wherein the solid oxide fuel cell operates at a temperature ranging between 400°C and 800°C.
- 5 19. Method according to claim 18 wherein the solid oxide fuel cell operates at a temperature ranging between 500°C and 700°C.
  - 20. Method according to claim 17 wherein the fuel is hydrogen.
  - 21. Process for preparing a solid oxide fuel cell including a cathode, an anode and at least one electrolyte membrane disposed between said anode and said cathode, wherein said anode comprises a cermet including a metallic portion and an electrolyte ceramic material portion; said process comprising the steps of:
    - providing a cathode;

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- providing the at least one electrolyte membrane; and
- providing an anode
- wherein the step of providing the anode includes the steps of:
  - a) providing a precursor of the metallic portion, said precursor having a particle size ranging between 0.2  $\mu m$  and 5  $\mu m;$
  - b) providing the electrolyte ceramic material having a particle size ranging between 1  $\mu m$  and 10  $\mu m$ ;
- 20 c) mixing said precursor and said ceramic material to provide a starting mixture;
  - d) heating and grinding said starting mixture in the presence of at least one first dispersant;
  - e) adding at least one binder and at least one second dispersant to the starting mixture from step d) to give a slurry;
- 25 f) thermally treating said slurry to provide a pre-cermet:
  - g) reducing the pre-cermet to provide the cermet.

- 22. Process according to claim 21 wherein the slurry resulting from step e) is applied on the electrolyte membrane.
- 23. Process according to claim 21 wherein the precursor of the metallic portion is an oxide.
- 5 24. Process according to claim 23 wherein the oxide is a copper oxide.
  - 25. Process according to claim 23 wherein the oxide is CuO.
  - 26. Process according to claim 21 wherein the precursor has a particle size ranging between 1 and 3  $\mu m$ .
- 27. Process according to claim 21 wherein the ceramic material has a particle size ranging between 2 and 5  $\mu m$ .
  - 28. Process according to claim 21 wherein step d) is carried out more than one time.
  - 29. Process according to claim 21 wherein the at least one first and second dispersants are selected from ethanol and isopropanol.
- 30. Process according to claim 21 wherein the at least one first dispersant is the same of the at least a second dispersant.
  - 31. Process according to claim 21 wherein the binder is soluble in the at least a second dispersant.
  - 32. Process according to claim 21 wherein the binder is polyvinylbutyral.
- 33. Process according to claim 21 wherein step f) is carried out at a temperature ranging between 700°C and 1100°C.
  - 34. Process according to claim 33 wherein step f) is carried out at a temperature ranging between 900°C and 1000°C.
  - 35. Process according to claim 21 wherein step g) is carried out at a temperature ranging between 300°C and 800°C.
- 36. Process according to claim 35 wherein step g) is carried out at a temperature ranging between 400°C and 600°C.

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- 37. Process according to claim 21 wherein step g) is performed with hydrogen containing from 1 vol.% to 10 vol.% of water.
- 38. Process according to claim 37 wherein hydrogen contains from 2 vol.% to 5 vol.% of water.
- 5 39. Cermet including a metallic portion and an electrolyte ceramic material portion, said portions being substantially uniformly interdispersed, said metallic portion having a melting point equal to or lower than 1200°C; said cermet having a metal content higher than 50 wt%, and a specific surface area equal to or lower than 5 m²/g.